<u>Annex – Dry lab iGEM Toulouse 2021</u>

> Model assumptions

- The different phases (liquid and gas) contained in the reactor are homogenous.
- O₂ produced by the cyanobacteria through photosynthesis coupled to the air bubbling in the reactor should result in saturated concentration of O₂ in the liquid phase, hence O₂ is considered as non-limiting, and its transfer is not included in the model. This hypothesis was verified during our bioreactor experiment.
- At each time interval, each microorganism must be in a state of metabolic equilibrium, hence the stoichiometric modelling. This assumption is justified by the fact that the time intervals are very small and that the overall dynamics of the system can therefore be considered as a succession of infinitesimal stationary states.

> Details of parameter calculation

CO2 concentration of the gas input CO₂^{gas}in
We use the ideal gas law to calculate this concentration:

PV=nRT

\rightarrow CO₂^{gas}in= n/V=P/RT=41 mM

At atmospheric pressure and 35°C.

Production yield of sucrose R_{CO2,Sucrose}

In the work carried out by (Lin et al. 2020), the authors were able to measure that for the sucrose-secreting strain *S. elongatus UTEX 2973* CscB, approximately 80% on average of the fixed CO2 goes to sucrose upon induction.

Hence: R_{CO2, Sucrose} = 0,8 Cmole sucrose / Cmole CO2 = 0,067 mmol sucrose / mmol CO2

Production yield of the violet leaf aldehydes (nonadienal and nonadienol)

The precursors of these molecules is alpha-linolenic acid (ALA). Under optimized conditions, it was shown that *S. elongatus* can reach a lipid content of $29.0 \pm 2.1\%$ w/w (Silva et al. 2014). This means that the one gram of biomass contains 290 mg of lipids.

Moreover, approximately 3.5% of these lipids are ALA (Santos-Merino et al. 2018). There is therefore 10,15 mg ALA/gDCW. By assuming that all this precursor will be consumed in the LOX pathway and using the growth rate of *S. elongatus UTEX 2973*, we find:

q_{nonadienol/al}= 0,012 mmol/gDCW/h

We finally divide this result by the maximum uptake rate of CO₂ which gives:

R_{CO2,Nonadienol/al} = 0,00032 mmol nonadienal / mmol CO2

Production yield of the violet terpenes

Due to the strong link of our dry lab work and our Supporting Entrepreneurship section, we chose to be as close as possible of an industrial production framework. The highest lycopene producing yeast strain described to date is able of accumulating 73.3 mg/g DCW (Ma et al. 2019).

By multiplying this by the growth rate of our strain (0,5 h⁻¹), we obtain: $q_{lycopene}=0,00745 \text{ mmol/gDCW/h}$

We split this between the four terpenes (and normalize with the carbon number of each molecule).

q_{alpha_ionone} =0,0171 mmol/gDCW/h q_{beta_ionone} = 0,0171 mmol/gDCW/h q_{dihydroionone} = 0,0171 mmol/gDCW/h q_{linalool} =0,0683 mmol/gDCW/h

We finally divide by q_{sucrose}max and obtain:

R sucrose, α ionone = 0,002 R sucrose, β ionone = 0,002 R sucrose, Dihydroionone = 0,002 R sucrose, Linglool = 0,008

References:

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